

# Experimental and Numerical Investigation of the Thermal Decomposition of Materials at Three Scales: Application to Polyether Polyurethane Foam Used in Upholstered Furniture

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Le progrès, une passion à partager

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# Presentation layout

## **1. Background and methodology**

2. Proposition of possible kinetic mechanisms
3. Determination of the kinetic mechanism and calculation of kinetic parameters
4. Small scale analysis (cone calorimeter)
5. Fire of simplified upholstered furniture
6. Conclusions and perspectives



# The current numerical approaches of fire

## The physics of fire

- Take only into account a **single stage** global decomposition **kinetic**
- **Extrapolate** the **phenomena** observed at the small scale to the large scale
- **Neglect** the **influence** of solid decomposition **kinetics** in the dynamic of combustion

## The chemistry of fire

- Consider **infinitely** fast chemical **reactions**
- **Restrict** strongly the number of species and **pollutants** entering into reaction
- **Tabulated** chemistry
- **Lack** of knowledge of the **transformation** of species in the **region** between the solid and the flame

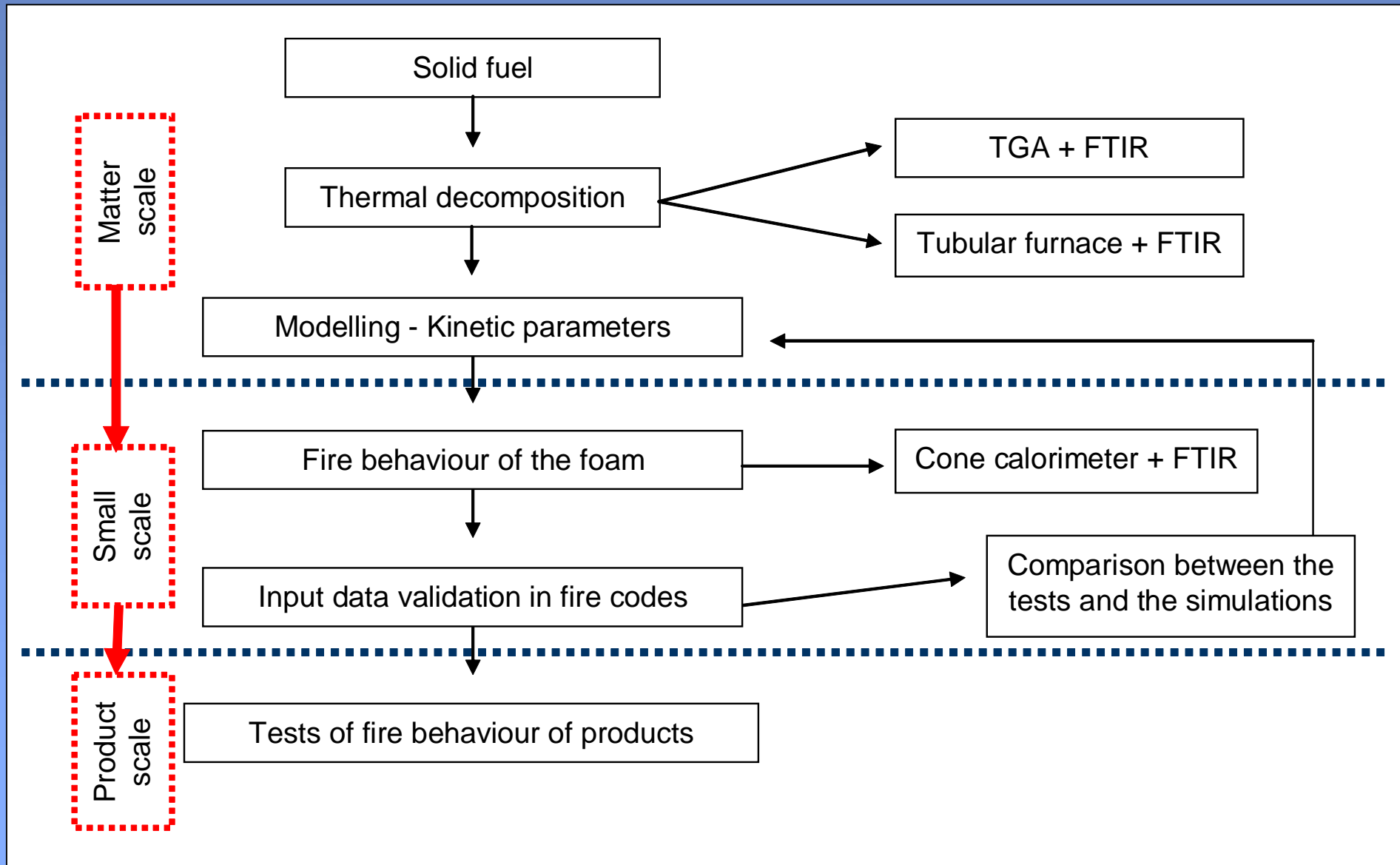


# Goal

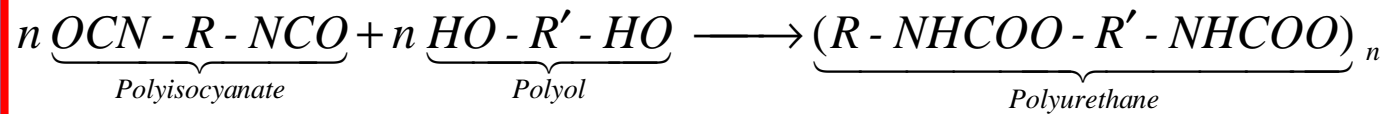
To develop a **general method** for establishing the **multi-stage** decomposition mechanism of **solid** materials based in a **multi-scale** analysis. The method is allowed to take into account the **chemistry** of the process (**pollutants** release).



# Methodology of the work



# Characterisation of the virgin foam

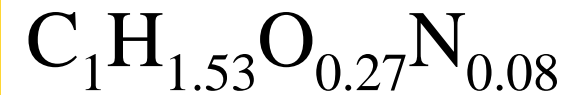


Source: Ohtani H. et al. (1987)

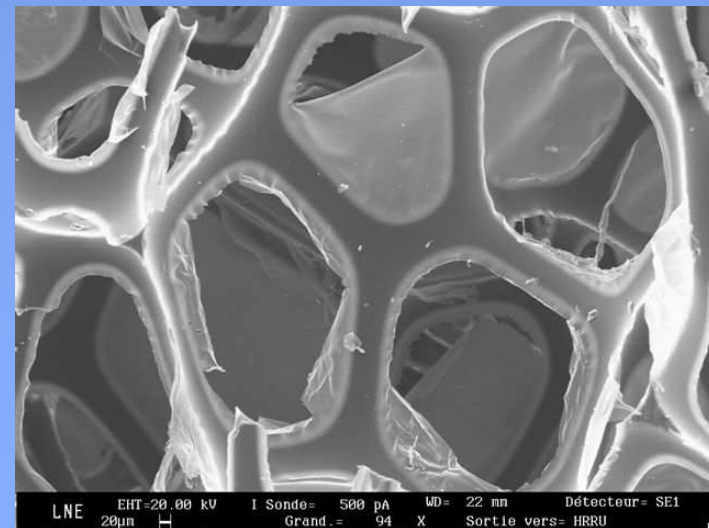
Element	Content
C	61.9%
H	8.5%
O	22.5%
N	5.9%
S	< 0.2%
Cl	< 10 ppm

Performed in Service central d'analyse

Molecule formula



Structure of virgin foam



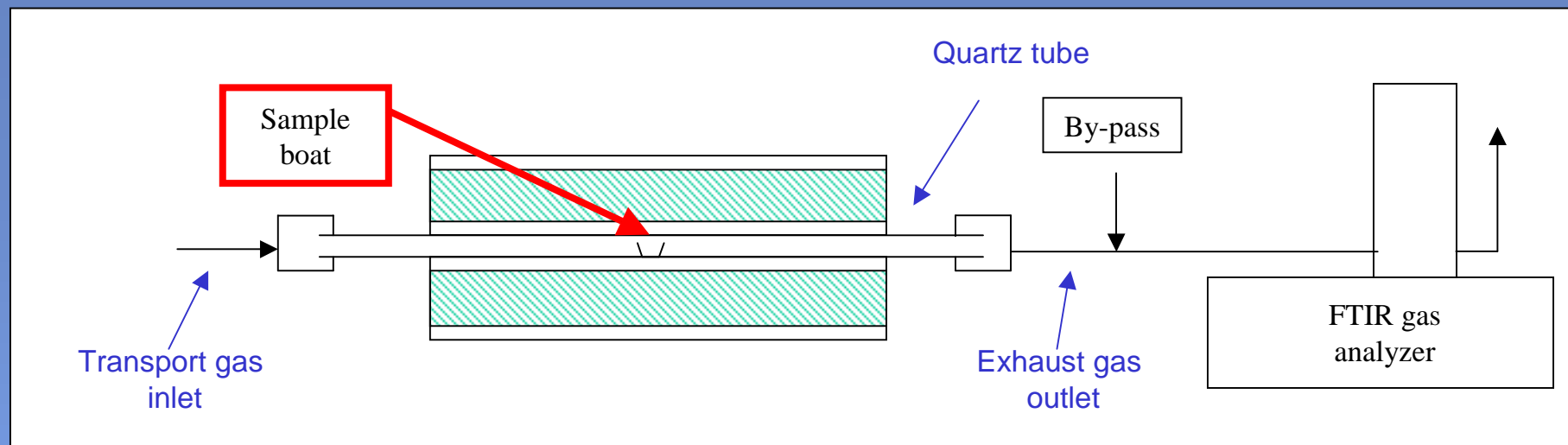
Density = 22 kg•m<sup>-3</sup>

Raw components from  
the manufacturer

Performed in LNE



# Tubular furnace and FTIR



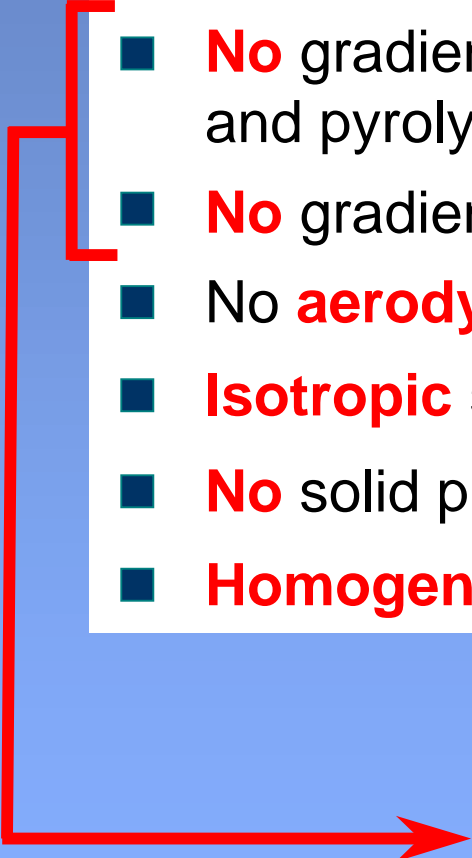
Calibrated product		Quantification limits [ppm]	
Component	Symbol	Low	High
Carbon monoxide	CO	2.5	8802
Carbon dioxide	CO <sub>2</sub>	260.4	101100
Water	H <sub>2</sub> O	21.1	22560
Nitrogen monoxide	NO	4.9	883
Nitrogen dioxide	NO <sub>2</sub>	1.0	639
Nitrous oxide	N <sub>2</sub> O	8.5	1005
Hydrogen cyanide	HCN	5.0	1020
Hydrogen chloride	HCl	2.1	5290
Hydrogen bromide	HBr	2.0	1000
Methane	CH <sub>4</sub>	0.3	4990
Acetylene	C <sub>2</sub> H <sub>2</sub>	2.1	994
Ethylene	C <sub>2</sub> H <sub>4</sub>	2.7	995
Formaldehyde	H <sub>2</sub> CO	21.7	131
Sulfur dioxide	SO <sub>2</sub>	1.0	852
Ammonia	NH <sub>3</sub>	1.0	1085



# Matter scale hypotheses

## Particles

- Masses **< 110 mg**
- **No** gradients of **concentration** of oxygen and pyrolysis products
- **No** gradient of **temperature**
- No **aerodynamics** effects around the particle
- **Isotropic** structure
- **No** solid phase **transport** effects
- **Homogeneous** decomposition of samples



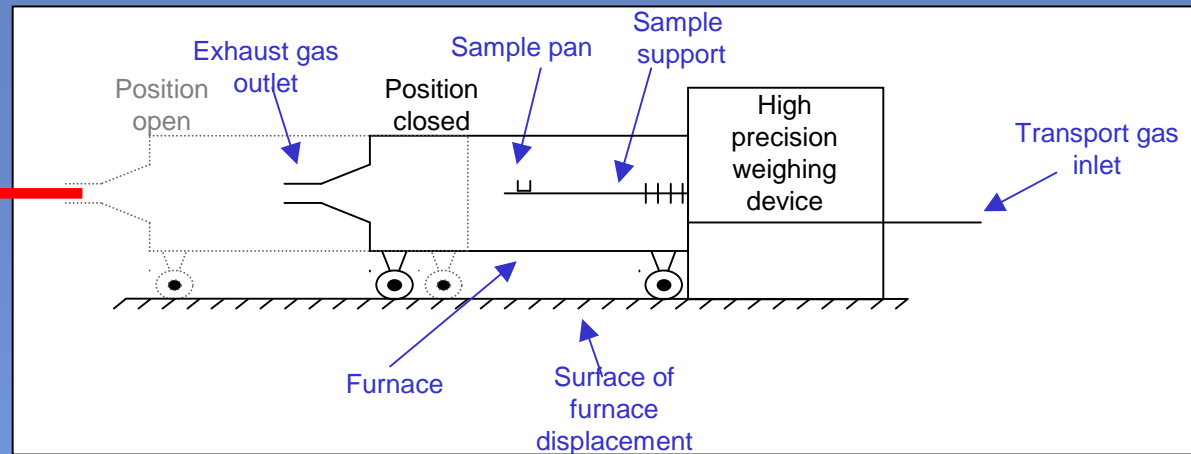
**Alveolar** matrix of PPUF, high **effective** exchange area





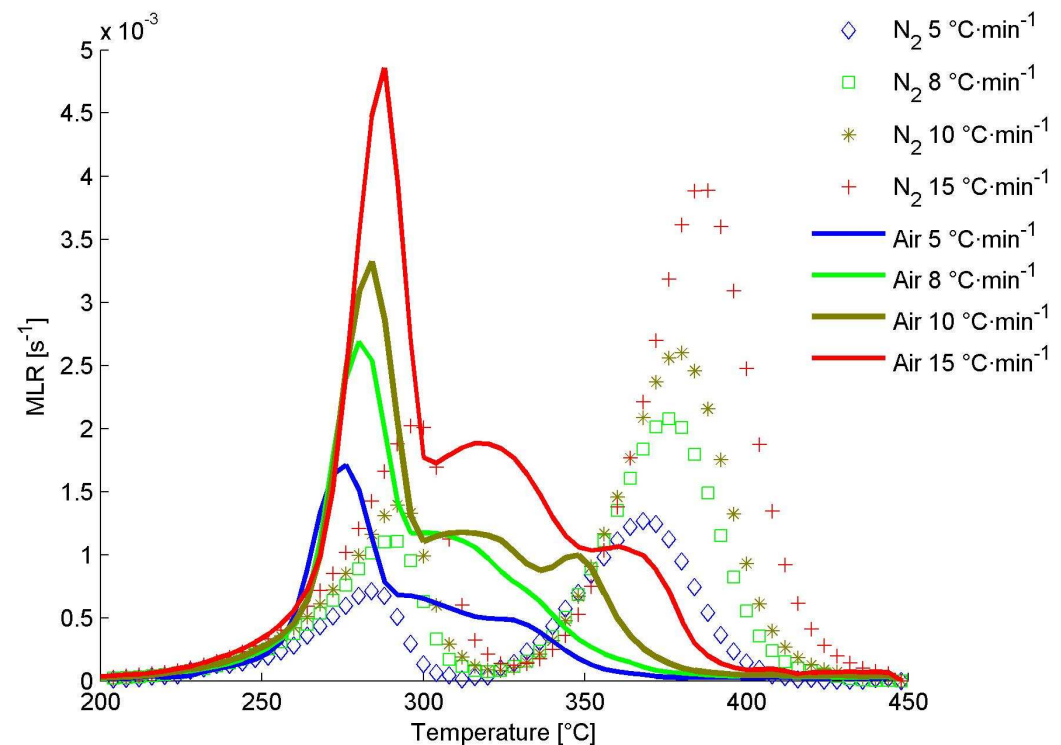
# TGA experiments

To  
FTIR



Heating rates:  
Found in literature  
Stages separation  
No gradients\*

\*Source: Lachaud J. et al. (2008)



# Methodology of Modelling



Total mass at time t, is the sum of remaining mass of each condensed phase species

$$\frac{dm(t)}{dt} = \frac{dm_{PPUF}}{dt} + \frac{dm_{polyol}}{dt} + \frac{dm_{char}}{dt} + \frac{dm_{residue}}{dt}$$

Each equation has an Arrhenius reaction rate

$$\dot{\omega}_i = A_i e^{-\frac{E_i}{RT}} \left( \frac{m_i}{m_o} \right)^{n_i} Y_{O_2}^{\delta}$$

$$MLR_i = \frac{dm_i}{dt} = v_i \cdot \dot{\omega}_i$$

Mass balance is expressed in terms of reaction rates and stoichiometric coefficients ( $v_i$ )

$$\frac{dm(t)}{dt} = \sum_{i=1}^5 (v_i - 1) \dot{\omega}_i$$

Calculation results are compared to experiments



# Coupling of solid and gas phases

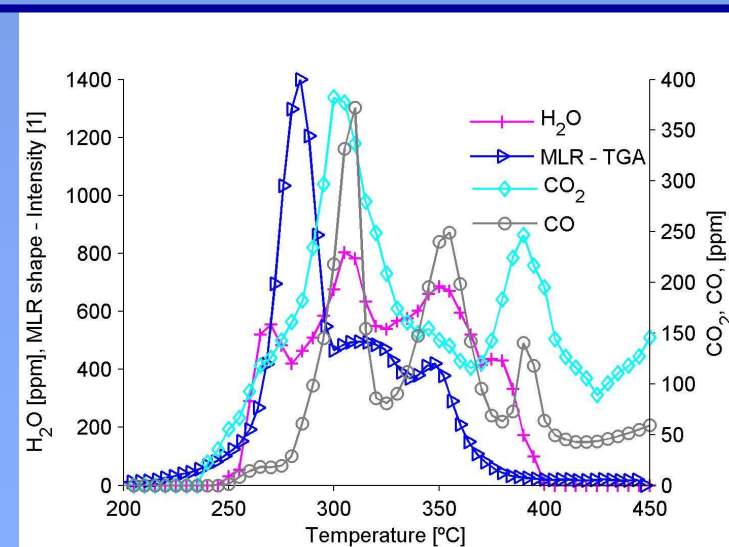
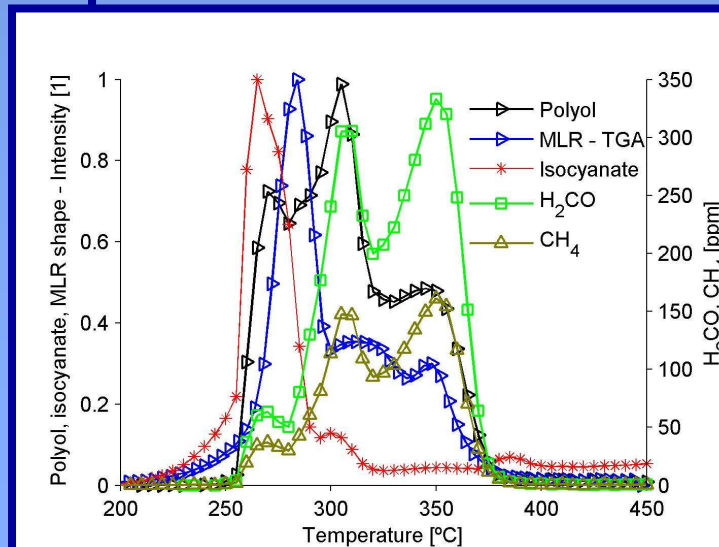
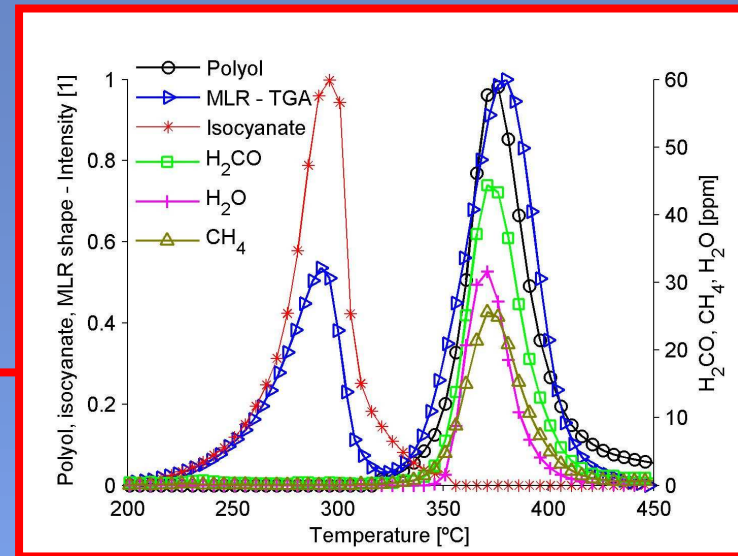
TGA data (**solid** phase)

+

FTIR data (**gas** phase)

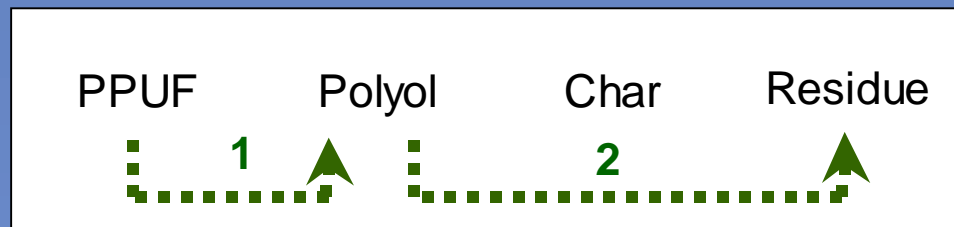
Nitrogen

Air



# Mechanism

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## Pyrolysis reactions

- **Isocyanate** is released during the **collapse** of PPUF
- **Polyol** remains in the holder as a **semi-liquid**
- The **residue** of the second reaction is **negligible**

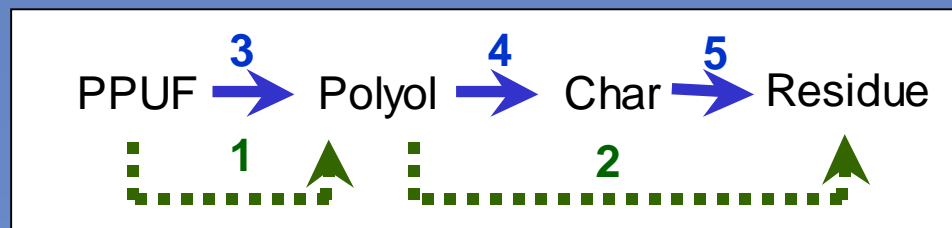
## Oxidization reactions

- The virgin PPUF decomposition is **shifted towards low temperature** in comparison to pyrolysis one, releasing gases formed only by diphasic reactions.
- The **gas products** evidence that the second oxidization reaction occurs in **lean O<sub>2</sub> atmosphere**
- **CO and CO<sub>2</sub>** appears during the **third** oxidization reaction. They are **not** present in the **pyrolysis** at a similar temperature (347 °C).



# Mechanism

13



## Pyrolysis reactions

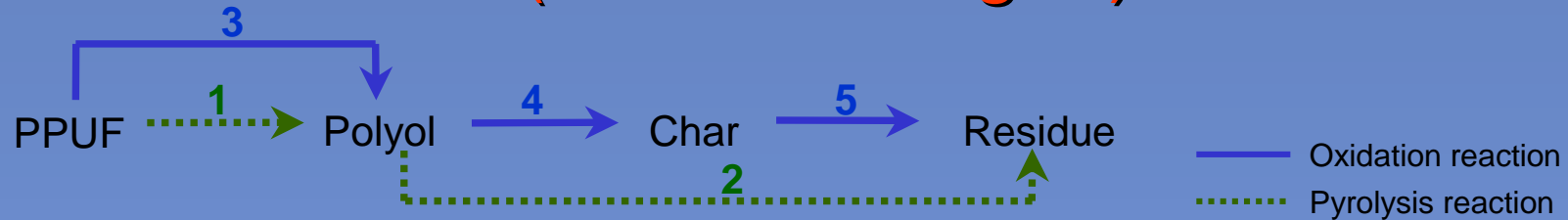
- Isocyanate is released during the collapse of PPUF
- Polyol remains in the holder as a semi-liquid
- The residue of the second reaction is negligible

## Oxidization reactions

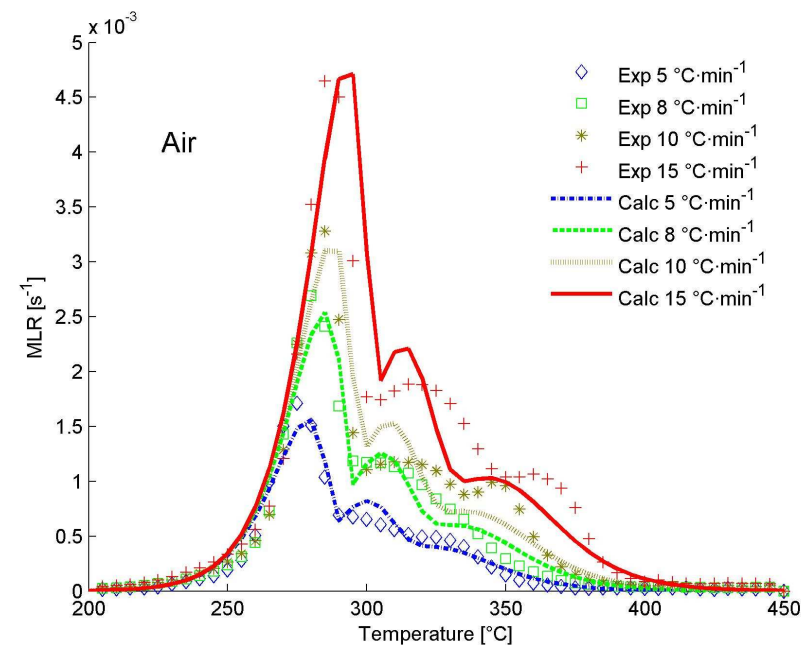
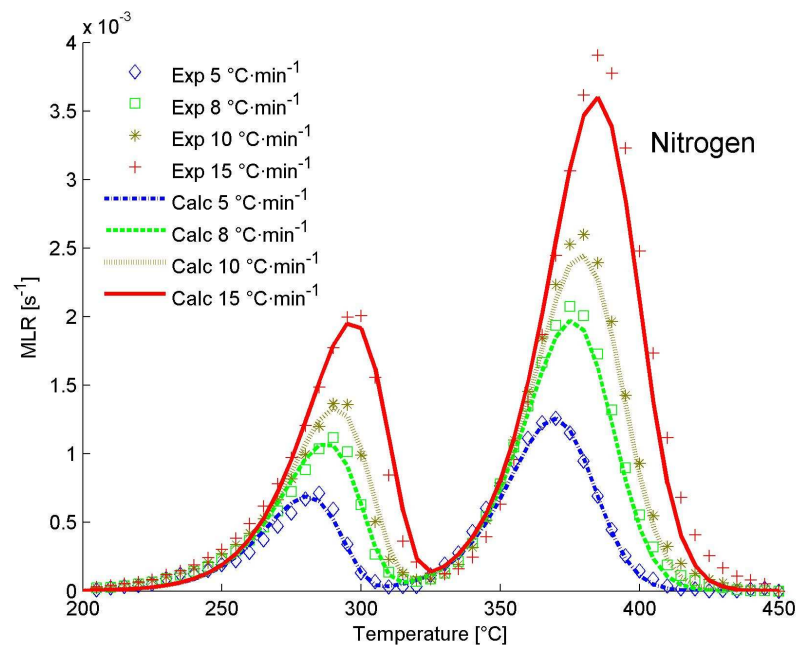
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# Prediction of MLR (air and nitrogen)



The kinetic parameters are dependent of the **evaluation function** and the decomposition **mechanism**.

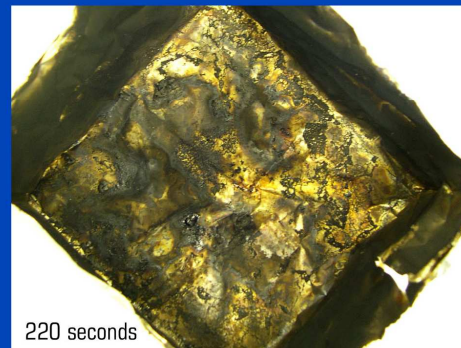
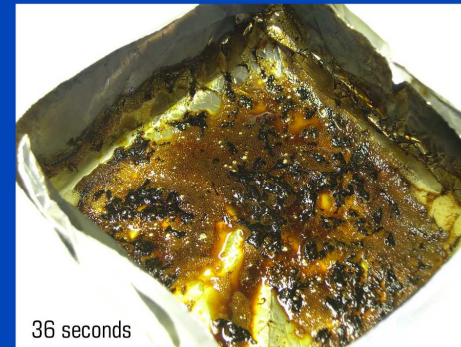


The **kinetic parameters** that allows prediction of TGA experimental results are calculated using genetic algorithms.



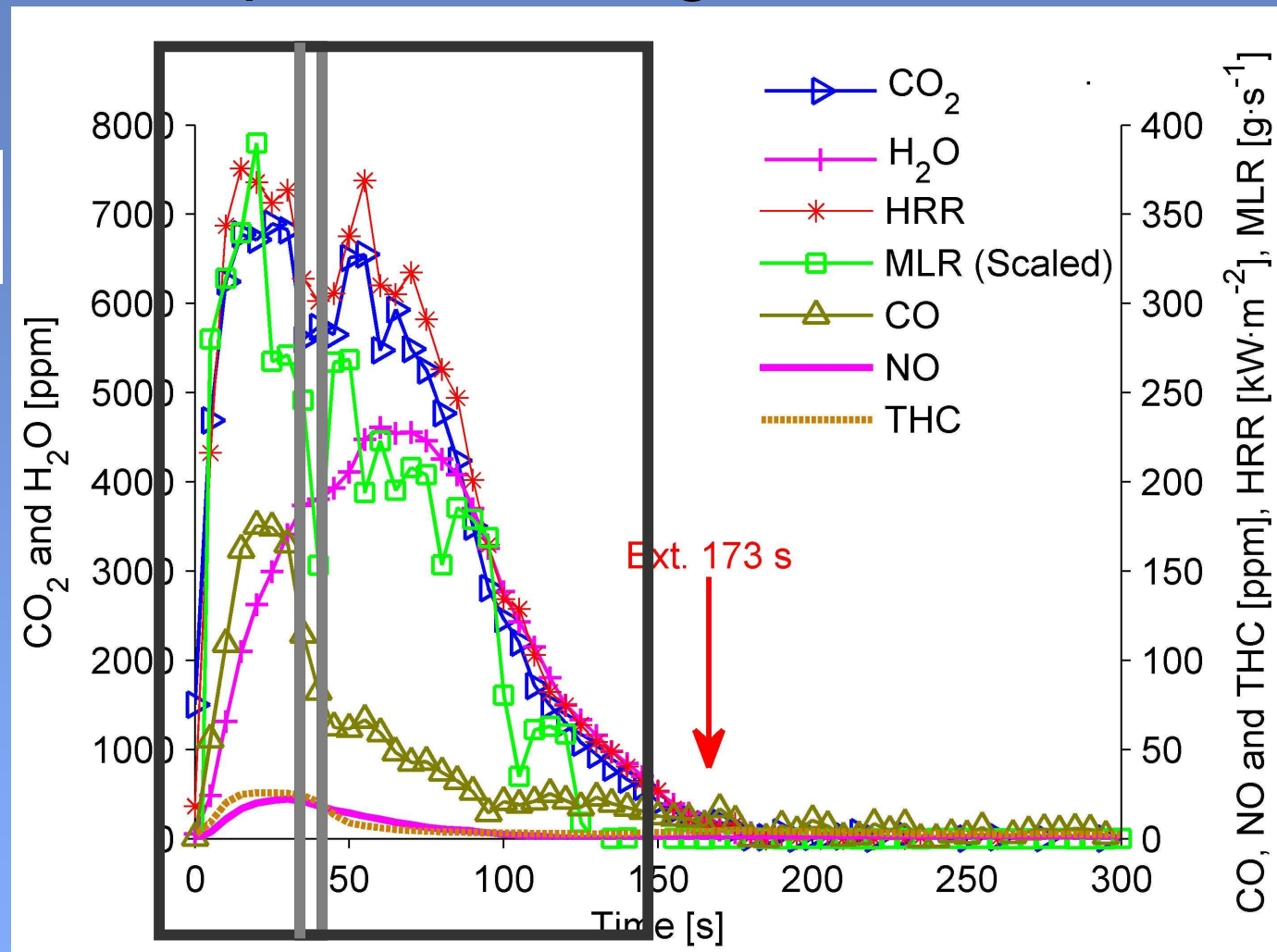
# The change of the solid phase

**30 kW·m<sup>-2</sup>**



# MLR & HRR coupled to toxic gases release

50 kW·m<sup>-2</sup>



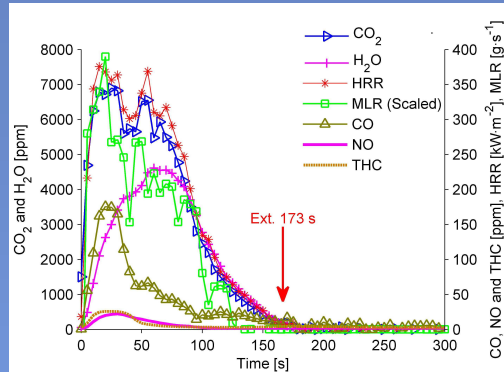
The release of **toxic gases** in function of time allows **analysis** of decomposition **mechanism** in CC

Source: Bustamante Valencia L. *et al.* Fire Safety Journal 44 (2009) 933 - 940





# Decomposition mechanism of PPUF in CC



32%Wt

68%Wt

PPUF  
↓  
Isocyanate  
+  
Polyol

**First** pyrolysis and  
combustion stage.  
Yellow smoke

**Second** pyrolysis  
and combustion  
stage  
Semi-liquid polyol

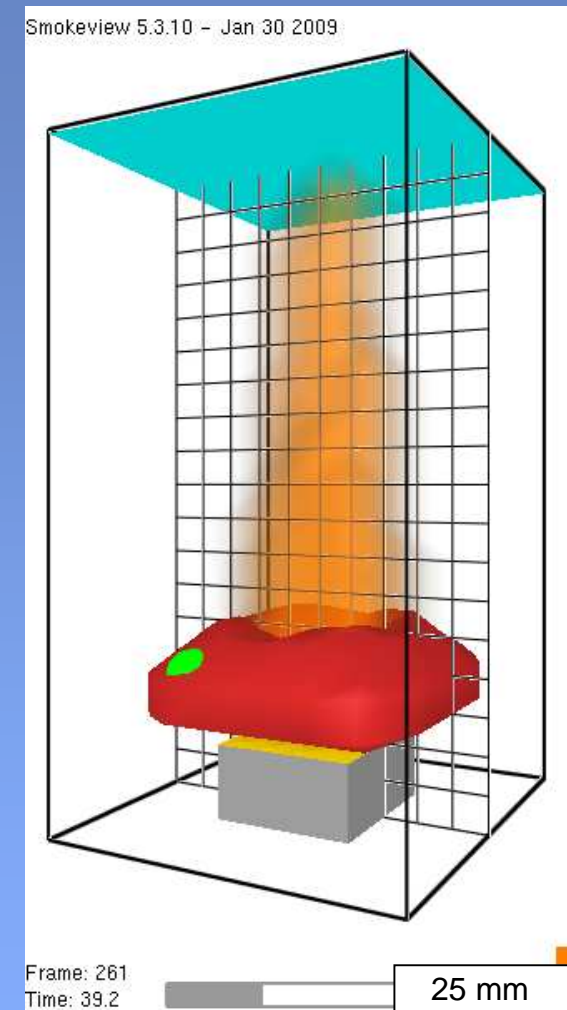
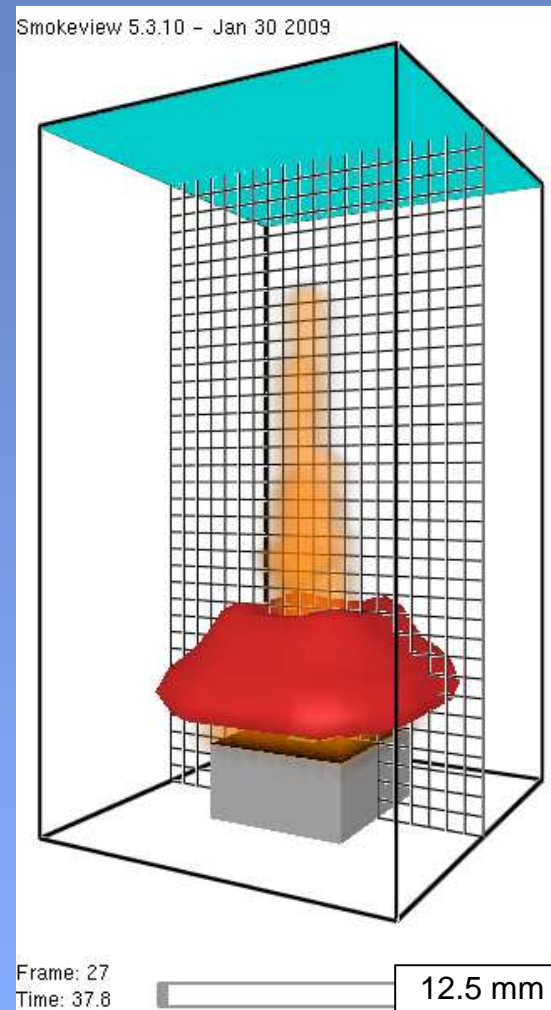
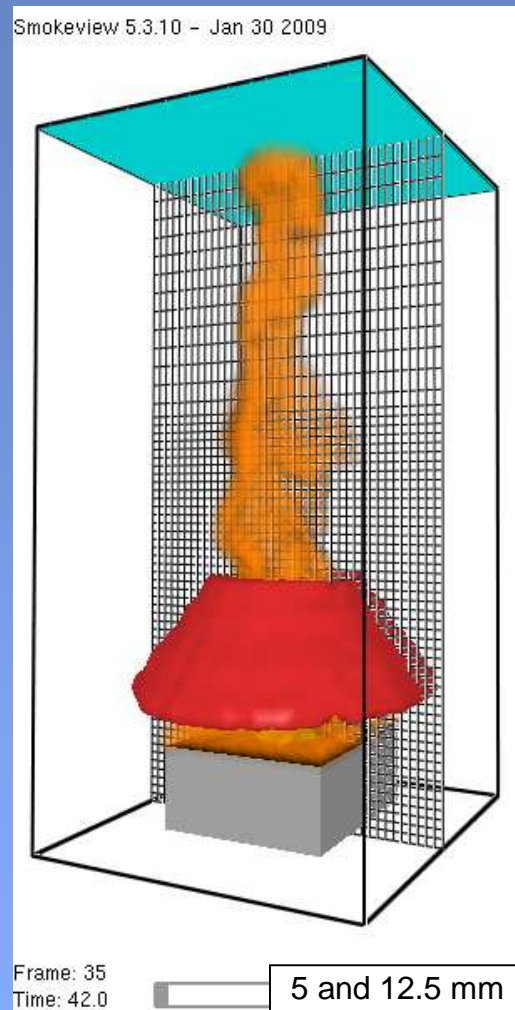
- The decomposition mechanism is in **accordance** to data from **matter scale and literature**

*Saunders et al. (1961), Woolley et al. (1972), Rogers et al. (1981).*

- The combustion of isocyanate and polyol are **not** completely **separated** in time.



# FDS simulations



**Three grid sizes** have been analysed, nevertheless the uncertainty of **input data** is priority.



# FDS simulations (2)

## Input data

- The pyrolysis calculated numerical simulations require as input data the **kinetic parameters** of the reaction and the **thermal properties**
- Very **few** pyrolysis calculated numerical simulations are find in the **literature**.
- The **thermal properties** can be specified as **vectors** in function of the temperature.
- A great **uncertainty** exists about how to **specify** the input data for the pyrolysis submodels.

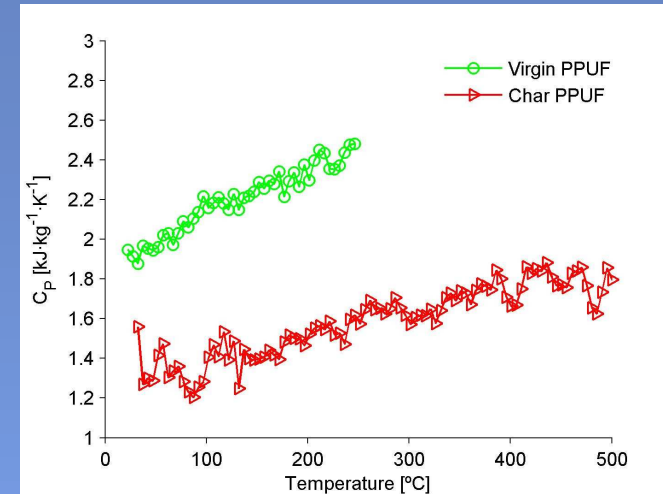


# Thermal properties

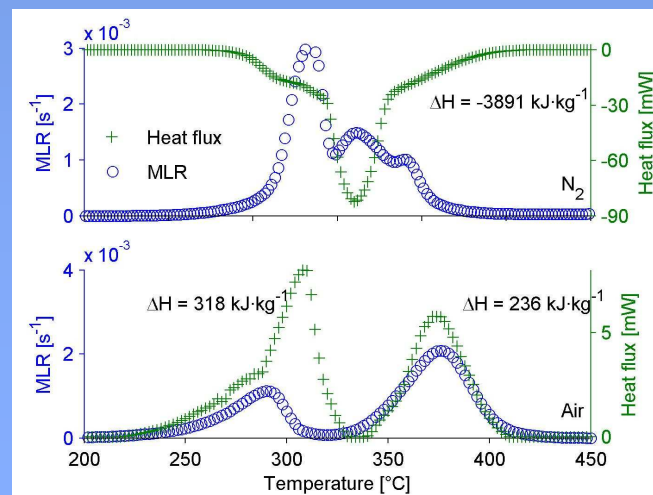
Input data for numerical simulations

$$\Delta H_{\text{c gross}} = 29.8 \text{ MJ} \cdot \text{kg}^{-1}$$

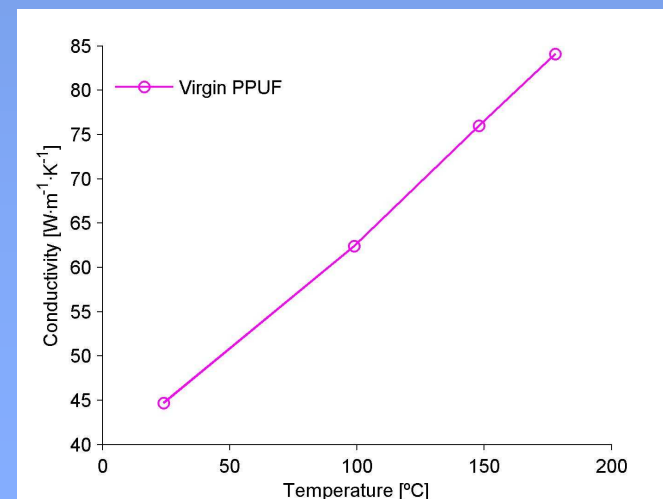
## Specific heat



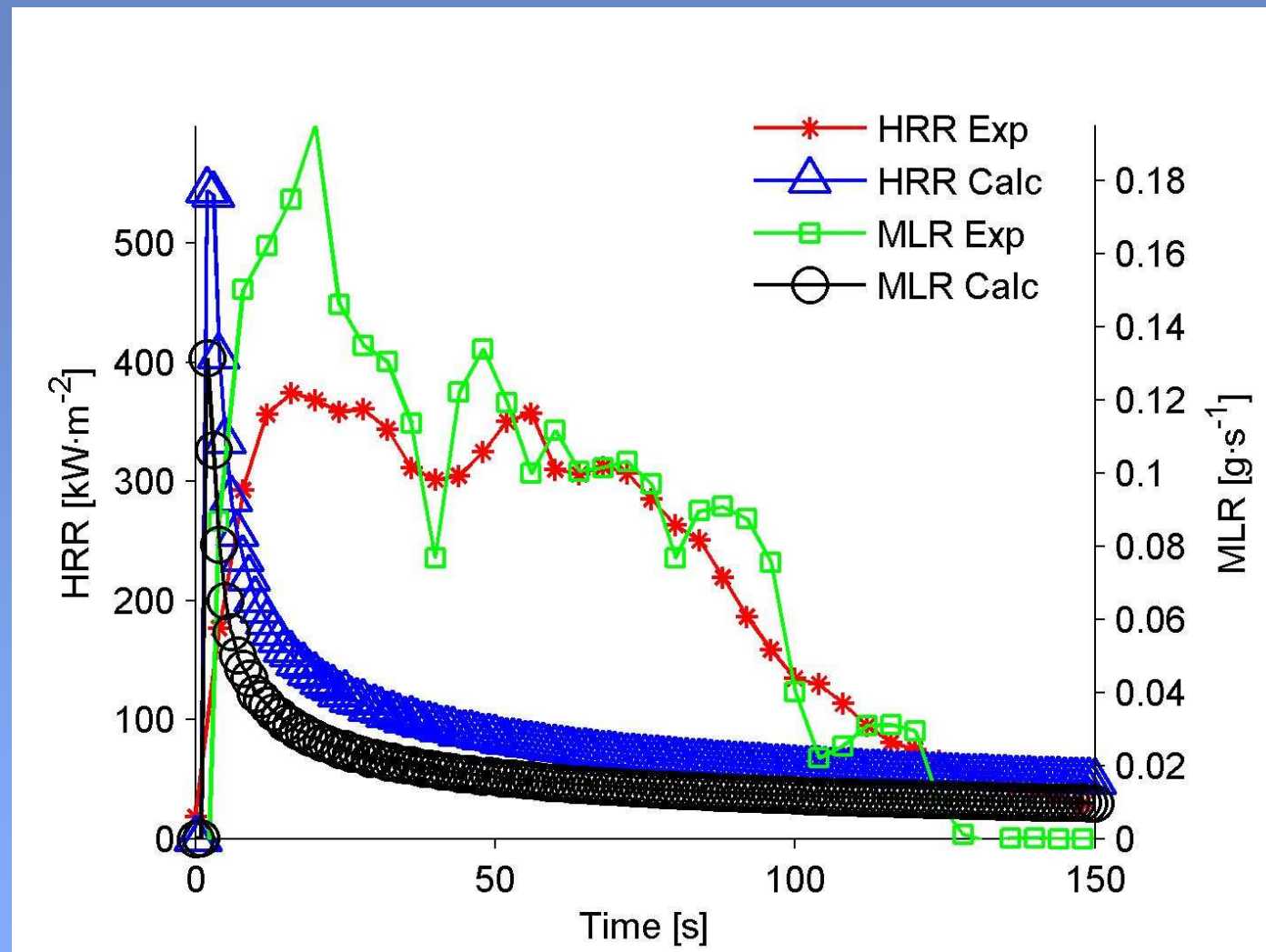
## Heat of reaction



## Thermal conductivity



# Experimental and calculated MLR and HRR



- Input data found in this research
- Simulations highly sensible to remaining **residue**

# Discussions

## Lack of accuracy of the simulations

- **Sensitivity** analyses of multi-stage decomposition schemes are required.
- **No** diphasic reactions with **oxygen** are allowed
- The **conduction model** does not take into account the change of state of the intermediary species
- Combined **uncertainty** about the kinetic parameters and the variable thermal properties
- Strong influence of the **properties of the residue** remained in the holder on the MLR output
- The **effective heat of combustion** per individual reaction is difficult to be determined (up to date)





# Fire of a piece of upholstered furniture



t = 70 s



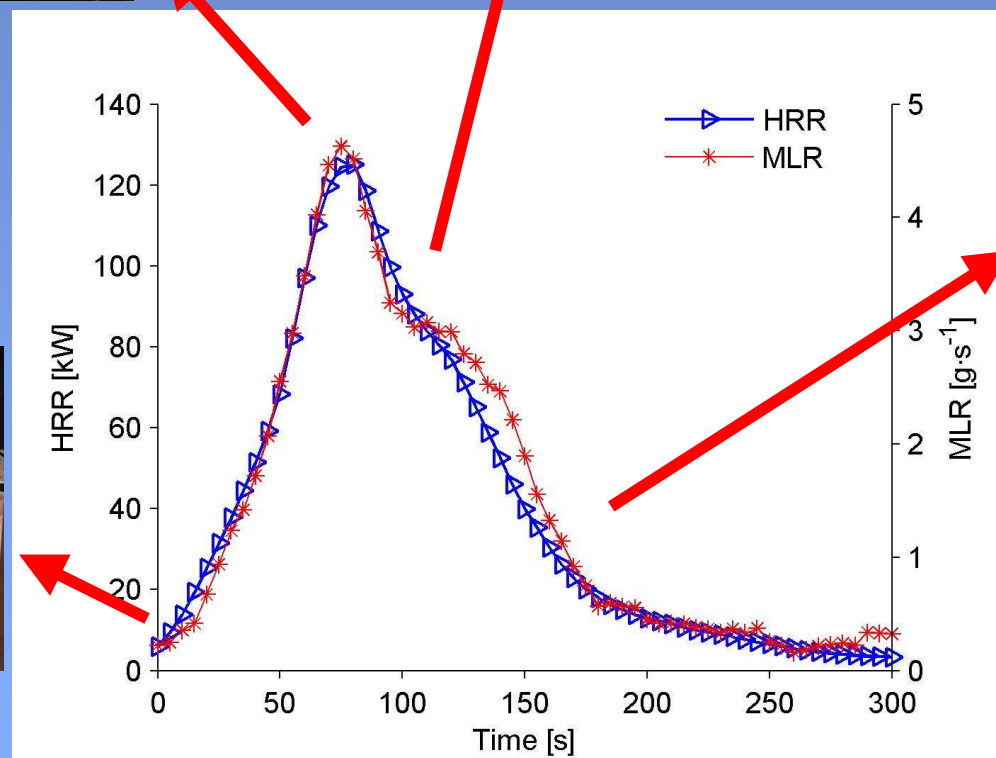
t = 120 s



t = 0 s

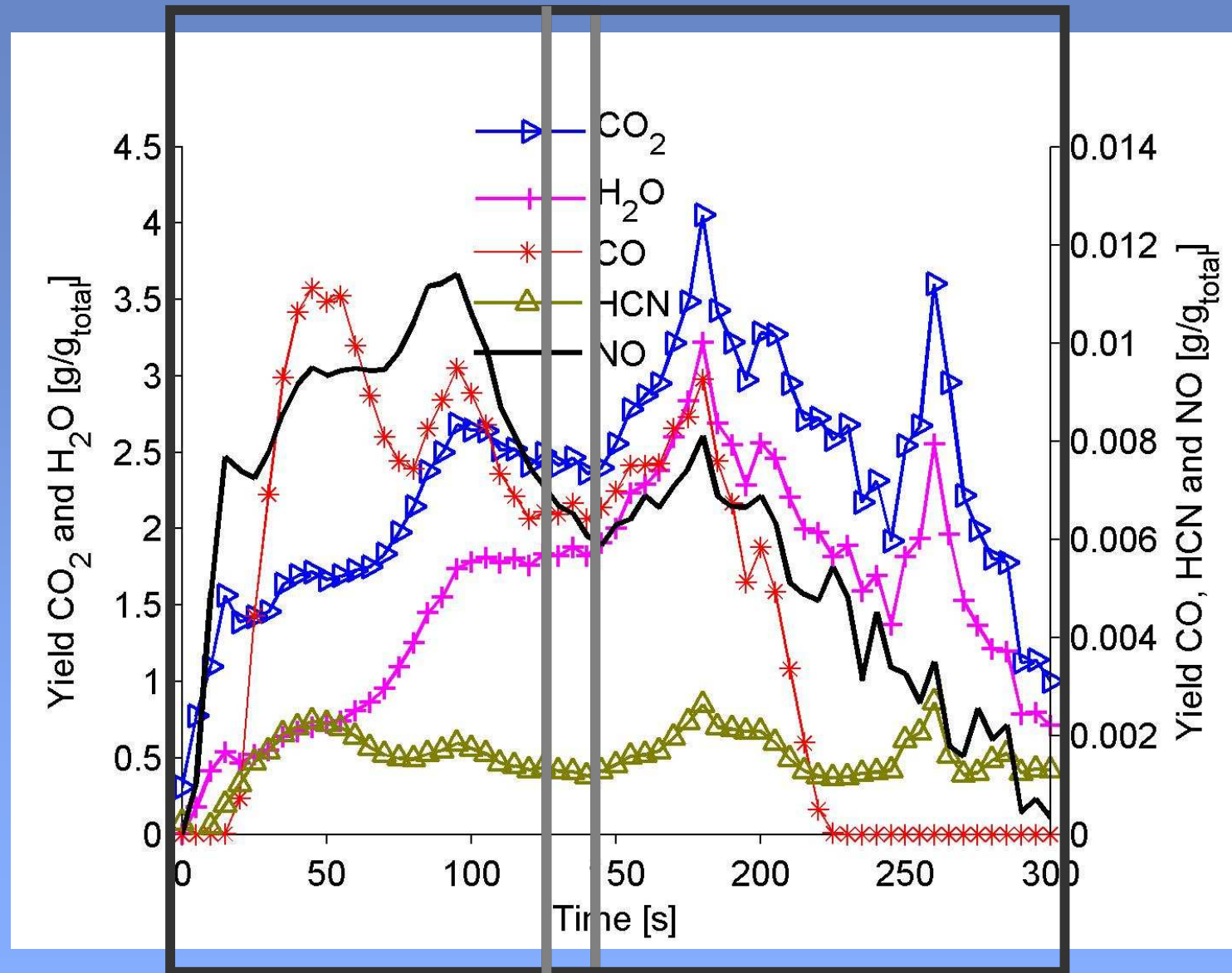


t = 180 s



The **same** decomposition **mechanism** of CC

# Fire of a piece of upholstered furniture





# Conclusion

- Information from the **solid and gas phase** was used to determine the **multi-stage** decomposition mechanism of PPUF
- The decomposition mechanism remained **unchanged** independently of the scale considered
- The **kinetic parameters** of the decomposition process were calculated allowing prediction of MLR
- The **pyrolysis models** of fire simulation codes need to be **improved** in order to predict accurately the behaviour of complex materials
- The **sensitivity** of input data need to be verified at various scales



# Perspective

- The **temperature distribution** in the matrix and in the surface (pyrolysis front) need to be determined accurately
- The influence of **oxygen** in the kinetic of decomposition need to be studied
- The **prediction** of the kinetic of release of **toxic gases** need to be improved
- Improvement of the **procedures** that allow the **measuring the input data** of fire simulation codes are required



Thank you very much!

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